1	WHA	AT IS CLAIMED IS:		
2				
3	1.	A process for producing stable lubricant bright stock comprising the		
4		steps	of:	
5				
6		a)	providing a petroleum residuum-derived stream having a sulfur	
7			content of less than 1% and a nitrogen content of less than	
8			0.5%;	
9				
10		b)	separating the residuum-derived stream at a distillation cut point	
11			in the range of 1150°F to 1300°F, into a heavy fraction and at	
12			least one light fraction;	
13				
14		c)	hydrocracking the at least one light fraction under lube	
15			hydrocracking in a lube hydrocracking zone in the presence of a	
16			hydrocracking catalyst and hydrogen under conditions to reduce	
17			the concentration of sulfur and nitrogen to suitable levels for	
18			hydroisomerization dewaxing; and	
19				
20		d)	dewaxing at least a portion of the hydrocracked stream in an	
21			hydroisomerization zone in the presence of a hydroisomerization	
22			catalyst and hydrogen under hydroisomerization conditions to	
23			produce a lubricant bright stock.	
24				
25	2.	The p	rocess of Claim 1, wherein the petroleum residuum-derived	
26		strear	n is a hydrocracked deasphalted oil.	
27				
28	3.	The p	rocess of Claim 1, wherein the petroleum residuum-derived	
29		strear	n is a hydrocracked residuum.	
30				
31	4.	The p	rocess of Claim 1, wherein the petroleum residuum-derived	
32		strear	n has a concentration of sulfur of less than 0.5% and a	
33		conce	entration of nitrogen of less than 0.2%.	

1	5.	The process of Claim 1, further comprising stabilizing the lubricant
2		bright stock in a hydrofinishing zone in the presence of a hydrofinishing
3		catalyst and hydrogen under hydrofinishing conditions.
4		
5	6.	The process of Claim 5, further comprising contacting the stabilized
6		lubricant bright stock with clay in a clay treatment zone.
7		
8	7.	The process of Claim 1, wherein the bright stock has a viscosity,
9		measured at 100°C, of greater than 15 cSt and viscosity index of
10		greater than 80.
11		
12	8.	The process of Claim 7, wherein the bright stock has a viscosity index
13		of greater than 90.
14		
15	9.	The process of Claim 1, wherein the bright stock has a viscosity in the
16		range of 20 and 60 cSt, measured at 100°C.
17		
18	10.	The process according to Claim 1, wherein the hydroisomerization
19		catalyst is selected from the group consisting of SAPO-11, SAPO-31,
20		SAPO-41, SM-3, ZSM-22, ZSM-23, ZSM-35, ZSM-48, ZSM-57,
21		SSZ-32, offretite, ferrierite and combinations thereof.
22		
23	11.	The process according to Claim 10, wherein the hydroisomerization
24		catalyst is selected from the group consisting of SAPO-11, SAPO-31,
25		SM-3, SSZ-32, and ZSM-23.
26		
27	12.	The process according to Claim 11, wherein the hydroisomerization
28		catalyst is selected from the group consisting of SAPO-11, SM-3,
29		SSZ-32, and ZSM-23.
30		
31	13.	The process according to Claim 1, wherein the hydroisomerization

catalyst has a metal hydrogenation component.

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The process according to Claim 13, wherein the metal hydrogenation 1 14. 2 component is platinum, palladium, or a mixture thereof. 3 4 15. The process according to Claim 10 wherein the metal hydrogenation 5 component is platinum. 6 7 16. The process according to Claim 1, wherein the suitable levels for 8 hydroisomerization dewaxing include a concentration of nitrogen of 9 less than 50 ppm and a concentration of sulfur of less than 100 ppm. 10 11 17. The process according to Claim 1, wherein the suitable levels for 12 hydroisomerization dewaxing include a concentration of nitrogen of 13 less than 30 ppm and a concentration of sulfur of less than 50 ppm. 14 15 18. The process according to Claim 1, wherein the suitable levels for 16 hydroisomerization dewaxing include a concentration of nitrogen of 17 less than 10 ppm and a concentration of sulfur of less than 20 ppm.